

## FDM SIMULATION OF Cu–Al<sub>2</sub>O<sub>3</sub>/WATER CASSON HYBRID NANOFLUID FLOW AND THERMAL TRANSPORT IN A COUETTE SYSTEM

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This paper numerically inspects the unsteady Couette Casson hybrid nanofluid (HNF) containing copper (Cu) and aluminum oxide (Al<sub>2</sub>O<sub>3</sub>) nanoparticles dissolved in water. The upper wall is set in uniform motion, and the lower wall is taken as stationary and stretchable. Finite difference method (FDM) is used to integrate the governed nonlinear partial differential equations. The results are explored through streamlines, isotherms, Nusselt number and skin friction. The impact of key dimensionless numbers such as Grashof number, Biot number, stretching parameter, Casson parameter, and Eckert number on Cu–Al<sub>2</sub>O<sub>3</sub>–water HNF is discussed. The results disclose that the flow and heat transfer (HT) can be controlled considerably by the key parameters.

**Keywords:** Couette flow; Variable viscosity; Al<sub>2</sub>O<sub>3</sub>–H<sub>2</sub>O nanofluid; Biot number; Stretching parameter

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### 1. INTRODUCTION

In recent years, substantial attention has been garnered by non-Newtonian fluid flows because of their extensive applications in engineering, biomedical, and industrial processes. Casson fluid model is one to describe non-Newtonian behaviour and captures effectively the yield-stress characteristics of materials like paints, polymer solutions, blood, and printing inks. This model was first introduced by Casson [1] in 1959. Mukhopadhyay [2] analysed HT in Casson flow over a stretchable surface. Abd El-Aziz and Afify [3] inspected MHD Casson flow with entropy generation. Previous investigations [4–8] have addressed Casson fluid flow over stretching surfaces, porous media, and boundary layers under the influence of magnetic fields, thermal radiation, viscous dissipation, and entropy generation. Several authors [9–13] confirmed Casson rheology's role in predicting realistic non-Newtonian flow behaviour in different configurations. These studies demonstrate the effectiveness of the Casson model in capturing realistic non-Newtonian behaviour, however, most are restricted to steady or external boundary-layer flows.

In parallel, nanofluid technology introduced to enhance thermal transport properties by dispersing nanoparticles into base fluids, has become a significant development in modern HT enhancement [14]. Tiwari and Das [15] studied the nanofluid flow in square cavity. Mono-nanofluids have been widely explored for various geometries and thermal conditions [16–20]. More recently, HNFs are made by combining two or more types of nanoparticles. Due to the synergistic effects between different particle materials, they exhibit improved thermal performance. Such hybrid suspensions exhibit superior HT capability, stability, and regulable viscosity. Unlike mono-nanoparticle nanofluids, HNFs highly associated to cooling systems, energy systems, and process engineering. Studies on Al<sub>2</sub>O<sub>3</sub>–Cu/water and related hybrid nanofluids with radiation and porous effects have reported notable enhancements in thermal efficiency [21–25].

Couette flow, representing the motion of a viscous fluid lying in two parallel plates with one or both plates in relative motion, serves as a fundamental configuration for studying shear-driven transport phenomena. Attia et al. [26] studied how temperature dependent viscosity and thermal conductivity influence unsteady hydromagnetic Couette flow. Couette flow is further studied by several researchers [27–33]. Existing studies have largely focused on steady-state flows or single-nanoparticle suspensions. In many practical applications, including lubrication systems and transient electronic cooling, the flow and temperature fields are naturally unsteady. Therefore, unsteadiness is incorporated to capture the transient evolution of the system. These transient effects are particularly important for accurately describing the behaviour of non-Newtonian hybrid nanofluids. Zeeshan et al. [34] studied MHD Casson hybrid nanofluid over the shrinking sheet. Although recent works have investigated Casson hybrid nanofluids in various geometries [35–42], the combined effects of unsteadiness, Casson and hybrid nanoparticle dispersion within an internal Couette geometry remain insufficiently explored.

Recent research [43–47] has focused on Casson hybrid nanofluids, where two or more distinct nanoparticles are dispersed in a Casson base fluid to achieve superior thermophysical performance. However, most prior studies have been

limited to steady, external boundary-layer configurations such as stretching sheets or porous media, neglecting unsteady internal geometries like Couette channels. The effects of unsteadiness and HT for Casson HNF in a Couette configuration are still not well understood. Therefore, present study aims to address this gap by investigating unsteady Casson HNF flow and HT between parallel plates. This analysis contributes new insights into non-Newtonian hybrid thermal transport under confined geometries.

Motivated by this gap, the current work examines the unsteady Couette flow of a Casson HNF consisting of Copper (Cu) and alumina (Al<sub>2</sub>O<sub>3</sub>) nanoparticles dispersed in water. The upper wall of the channel is moving uniformly, while the lower wall is stationary and stretchable. A comprehensive mathematical formulation incorporating the impact of key dimensionless parameters such as the Casson parameter, Grashof number, Biot number, stretching parameter, and Eckert number is developed. The governing nonlinear partial differential equations are solved using a finite difference method (FDM) to elucidate the fluid flow and HT characteristics.

## 2. MATHEMATICAL FORMULATION

An unsteady, laminar, incompressible Casson HNF flow of Cu-Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O confined within two parallel plates is taken into account. The viscosity of the fluid is considered to be a function of temperature. To configure the model geometry, x-axis is aligned with the plate and the y-axis is oriented perpendicular to the plates, as shown in Figure 1. The lower plate is located at y=0, possesses a stretching velocity U<sub>0</sub>. The upper plate had convective cooling at y = h. And this flow is driven by a uniform pressure gradient located at the ends of the channel.

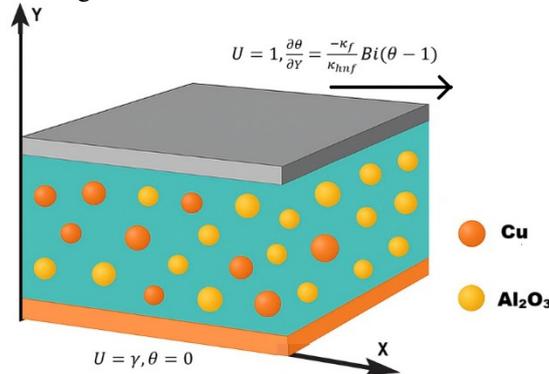


Figure 1. Physical configuration

Based on Tiwari and Das [15] nanofluid model for nanofluid, the governing equations are given by, Momentum equation:

$$\rho_{\text{hnf}} \frac{\partial u}{\partial \tau} = -\frac{\partial p}{\partial x} + \left(1 + \frac{1}{\lambda}\right) \frac{\partial}{\partial y} \left( \mu_{\text{hnf}}(T) \frac{\partial u}{\partial y} \right) + (\rho\beta_T)_{\text{hnf}} g(T - T_0) \quad (1)$$

Temperature equation:

$$\frac{\partial T}{\partial \tau} = \alpha_{\text{hnf}} \frac{\partial^2 T}{\partial y^2} + \frac{\mu_{\text{hnf}}(T) \alpha_{\text{hnf}}}{\kappa_{\text{hnf}}} \left( \frac{\partial u}{\partial y} \right)^2 \quad (2)$$

The dynamic viscosity is presumed to be an exponential declining function that depends on temperature [28], expressed as,

$$\mu_f(T) = \mu_0 e^{-m(T-T_0)} \quad (3)$$

Constraints at the boundary are:

$$\left. \begin{aligned} \text{When } \tau = 0, \quad u = 0, T = 0 \quad \text{at} \quad y = 0, y = h \\ \text{When } \tau > 0, \quad \left. \begin{aligned} u = U_0, T = T_0 \quad \text{at} \quad y = 0 \\ u = U_h, -\kappa_{\text{hnf}} \frac{\partial T}{\partial y} = h_f(T - T_\infty) \quad \text{at} \quad y = h \end{aligned} \right\} \end{aligned} \right\} \quad (4)$$

where U<sub>0</sub> corresponds to stretching velocity of bottom plate, U<sub>h</sub> denotes velocity of top plate, T<sub>∞</sub> depicts the ambient temperature, P represents nanofluid pressure. μ<sub>0</sub> symbolizes dynamic viscosity of nanofluid at reference temperature T<sub>0</sub> and m represents parameter of viscosity, h<sub>f</sub> symbolizes coefficient of HT. Volume fraction of comprised nanoparticles, density, thermal conductivity, thermal diffusivity and heat capacitance are described below. The subscripts f, s, nf and hnf refer to base fluid, solid nanoparticles, nanofluid and hybrid nanofluid. Relationships indicating the physical characteristics of nanofluids are expressed as:

$$\mu_{\text{hnf}} = \frac{\mu_f}{(1-\phi_1)^{2.5}(1-\phi_2)^{2.5}} \quad (5)$$

$$\rho_{hnf} = \left\{ (1 - \phi_2) \left( (1 - \phi_1) + \phi_1 \frac{\rho_{s1}}{\rho_f} \right) + \phi_2 \frac{\rho_{s2}}{\rho_f} \right\} \rho_f \tag{6}$$

$$(\rho C_p)_{hnf} = \left\{ (1 - \phi_2) \left( (1 - \phi_1) + \phi_1 \frac{(\rho C_p)_{s1}}{(\rho C_p)_f} \right) + \phi_2 \frac{(\rho C_p)_{s2}}{(\rho C_p)_f} \right\} (\rho C_p)_f \tag{7}$$

$$\kappa_{hnf} = \frac{(\kappa_{s2} + 2\kappa_f) - 2\phi_2(\kappa_f - \kappa_{s2})}{(\kappa_{s2} + 2\kappa_f) + \phi_2(\kappa_f - \kappa_{s2})} \kappa_{nf} \tag{8}$$

$$\kappa_{nf} = \frac{(\kappa_{s1} + 2\kappa_f) - 2\phi_1(\kappa_f - \kappa_{s1})}{(\kappa_{s1} + 2\kappa_f) + \phi_1(\kappa_f - \kappa_{s1})} \kappa_f \tag{9}$$

$$\alpha_{hnf} = \frac{\kappa_{hnf}}{(\rho C_p)_{hnf}} \tag{10}$$

**Table 1.** Thermophysical characteristics of Copper, Alumina and Water

Physical characteristics	Cu	Al <sub>2</sub> O <sub>3</sub>	H <sub>2</sub> O
C <sub>p</sub> (J/KgK)	385	765	4179
ρ (Kg/m <sup>3</sup> )	8933	3970	997.1
k (W/mK)	400	40	0.613

The following dimensionless quantities and parameters are invoked to change governing equations into non-dimensional form.

$$\left. \begin{aligned} X &= \frac{x}{h}, Y = \frac{y}{h}, U = \frac{hu}{v_f}, t = \frac{\tau v_f}{h^2}, \theta = \frac{T - T_0}{T_\infty - T_0}, Pr = \frac{v_f}{\alpha_f} \\ \bar{P} &= \frac{Ph^2}{\rho_f v_f^2}, \beta = m(T_\infty - T_0), Ec = \frac{v_f^2}{C_p(T_\infty - T_0)h^2}, Bi = \frac{h h_f}{\kappa_f}, \gamma = \frac{U_0}{h} \end{aligned} \right\} \tag{11}$$

The converted dimensionless equations could be written as:

$$\frac{\partial U}{\partial t} = \frac{\rho_f}{\rho_{hnf}} \left\{ -\frac{\partial \bar{P}}{\partial X} + \left( 1 + \frac{1}{\lambda} \right) \frac{\mu_{hnf}}{\mu_f} e^{-\beta\theta} \left[ \frac{\partial^2 U}{\partial Y^2} - \beta \frac{\partial \theta}{\partial Y} \frac{\partial U}{\partial Y} \right] \right\} + Gr \theta \tag{12}$$

Temperature equation:

$$\frac{\partial \theta}{\partial t} = \frac{(\rho C_p)_f}{(\rho C_p)_{hnf}} \left\{ \frac{1}{Pr} \frac{\kappa_{hnf}}{\kappa_f} \frac{\partial^2 \theta}{\partial Y^2} + \frac{\mu_{hnf}}{\mu_f} e^{-\beta\theta} Ec \left( \frac{\partial U}{\partial Y} \right)^2 \right\} \tag{13}$$

Boundary conditions are:

When  $t = 0$ ,  $U = 0, \theta = 0$  at  $Y = 0, Y = 1$

$$\left. \begin{aligned} U &= \gamma, \theta = 0 && \text{at } Y = 0 \\ U &= 1, \frac{\partial \theta}{\partial Y} = \frac{-\kappa_f}{\kappa_{hnf}} Bi(\theta - 1) && \text{at } Y = 1 \end{aligned} \right\} \tag{14}$$

Local coefficients of skin friction and Nusselt for lower and upper plates are given by

$$\left. \begin{aligned} C_{f0} &= \frac{\mu_{hnf}}{\mu_f} e^{-\beta\theta} \frac{\partial U}{\partial Y}_{Y=0}, C_{f1} = \frac{\mu_{hnf}}{\mu_f} e^{-\beta\theta} \frac{\partial U}{\partial Y}_{Y=1} \\ Nu_0 &= -\frac{\kappa_{hnf}}{\kappa_f} \frac{\partial \theta}{\partial Y}_{Y=0}, Nu_1 = -\frac{\kappa_{hnf}}{\kappa_f} \frac{\partial \theta}{\partial Y}_{Y=1} \end{aligned} \right\} \tag{15}$$

### 3. METHODOLOGY

The nonlinear coupled partial differential equations (12-13), with constraints (14), are evaluated numerically using finite difference method. Time derivative is computed with forward difference scheme and spatial derivatives of first and second order with central difference scheme. Convergence of the scheme is assumed when the values of unknowns  $U, \theta$  of two consecutive iterations differ by less than  $10^{-5}$  i.e.,  $|\varphi^{n+1} - \varphi^n| \leq 10^{-5}$ , where  $n$  specifies number of loops and  $\varphi$  stands for  $[U, \theta]^T$ . Table 2 shows the comparison of  $C_{f_{avg}}$  and  $Nu_{avg}$  of current study with previous works and found satisfactory.

Equations (12-13) could be written as:

$$\frac{\partial U}{\partial t} = A_1 + A_2 e^{-\beta\theta} \frac{\partial^2 U}{\partial Y^2} - A_3 e^{-\beta\theta} \frac{\partial \theta}{\partial Y} \frac{\partial U}{\partial Y} + A_4 \theta \tag{15}$$

$$\frac{\partial \theta}{\partial t} = B_1 \frac{\partial^2 \theta}{\partial Y^2} + B_2 e^{-\beta \theta} \left( \frac{\partial U}{\partial Y} \right)^2 \tag{16}$$

The explicit FDM scheme is given by,

$$U_i^{n+1} = U_i^n + \Delta t A_1 + \Delta t A_2 e^{-\beta \theta_i^n} \frac{U_{i+1}^n - 2U_i^n + U_{i-1}^n}{(\Delta Y)^2} - \Delta t A_3 e^{-\beta \theta_i^n} \left( \frac{\theta_{i+1}^n - \theta_{i-1}^n}{2\Delta Y} \right) \left( \frac{U_{i+1}^n - U_{i-1}^n}{2\Delta Y} \right) + \Delta t A_4 \theta_i^n \tag{17}$$

$$\theta_i^{n+1} = \theta_i^n + \Delta t \left[ B_1 \frac{\theta_{i+1}^n - 2\theta_i^n + \theta_{i-1}^n}{(\Delta Y)^2} + B_2 e^{-\beta \theta_i^n} \left( \frac{U_{i+1}^n - U_{i-1}^n}{2\Delta Y} \right)^2 \right] \tag{18}$$

Here

$$A_1 = -\frac{\rho_f}{\rho_{hnf}} \frac{\partial \bar{P}}{\partial X}, A_2 = \frac{\rho_f}{\rho_{hnf}} \left( 1 + \frac{1}{\lambda} \right) \frac{\mu_{hnf}}{\mu_f}, A_3 = \frac{\rho_f}{\rho_{hnf}} \left( 1 + \frac{1}{\lambda} \right) \frac{\mu_{hnf}}{\mu_f} \beta,$$

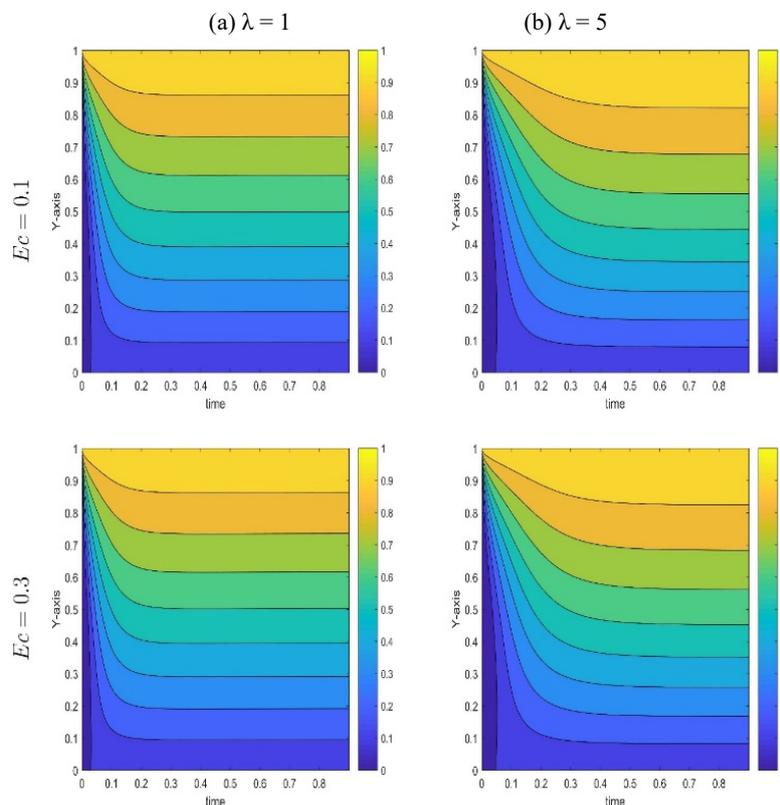
$$A_4 = Gr, B_1 = \frac{(\rho C_p)_f}{(\rho C_p)_{hnf}} \frac{1}{Pr} \frac{\kappa_{hnf}}{\kappa_f}, B_2 = \frac{(\rho C_p)_f}{(\rho C_p)_{hnf}} \frac{\mu_{hnf}}{\mu_f} Ec$$

**Table 2.** Comparison of Skin friction( $Cf_{avg}$ ) and Nusselt number( $Nu_{avg}$ ).

$\beta$	Bi	Ec	$Cf_{avg}$			$Nu_{avg}$		
			Ali and Makinde [28]	Karim et al. [29]	Current study	Ali and Makinde [28]	Karim et al. [29]	Current study
0.1	1	1.0	0.397	0.395	0.3962	0.512	0.511	0.5121
0.1	3	1.0	0.406	0.405	0.4058	0.790	0.784	0.7883
0.5	1	1.0	0.145	0.146	0.1443	0.223	0.221	0.2227
0.1	1	0.5	0.435	-	0.4347	0.039	-	0.0401
0.1	7	1.0	0.411	-	0.4106	0.943	-	0.9428

#### 4. DISCUSSION OF RESULTS

The governing nonlinear partial differential equations describing the unsteady Casson hybrid nanofluid flow were evaluated numerically using FDM. The impact of various non-dimensional numbers, namely the Casson parameter ( $\lambda$ ), Eckert number (Ec), Biot number (Bi), viscosity parameter ( $\beta$ ), nanoparticle volume fraction ( $\phi$ ), stretching parameter ( $\gamma$ ), and Grashof number (Gr) on velocity, temperature, skin friction, and Nusselt number are presented and interpreted in this section.



**Figure 2.** Streamlines for (a)  $\lambda = 1$  (b)  $\lambda = 5$  and  $Ec = 0.1, 0.3$

Figures 2 and 3 illustrate the streamline and isotherm patterns for different values of the Casson parameter  $\lambda$  and Eckert number  $Ec$ . It is noticed that with increasing  $\lambda$  (i.e., higher Casson parameter implying stronger yield stress), the flow resistance increases and the velocity gradients near the walls become weaker. Consequently, the flow field becomes more uniform and shear layers are reduced. The isotherm contours reveal that higher  $\lambda$  suppresses heat generation near the moving wall, leading to a more uniform temperature field. An increase in  $Ec$  enhances the internal viscous dissipation, which thickens the boundary layer of temperature and raises thermal profile throughout the channel.

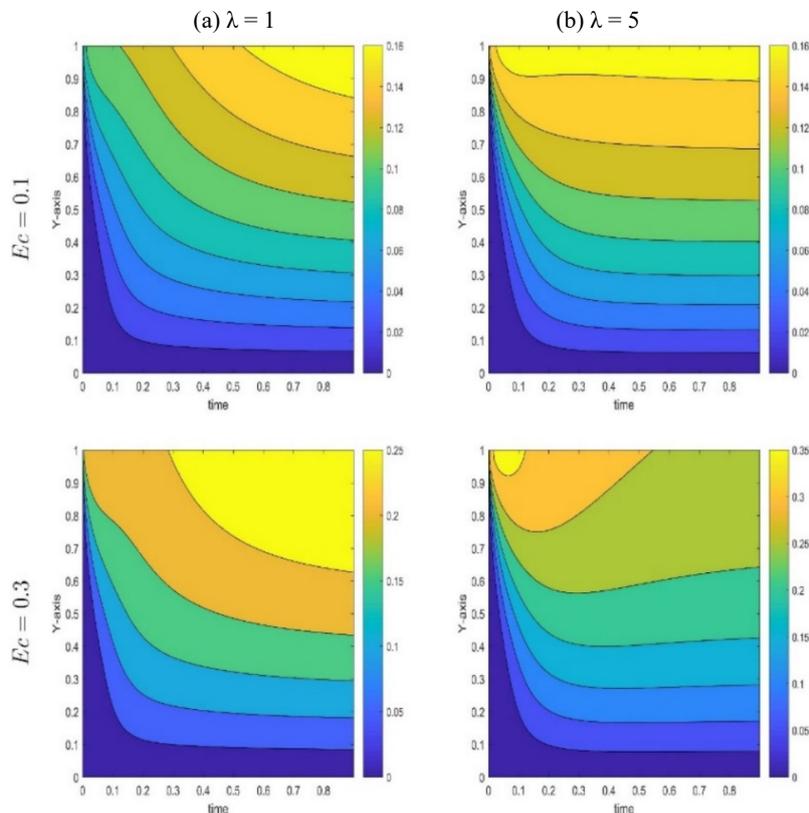


Figure 3. Isotherms for (a)  $\lambda = 1$  (b)  $\lambda = 5$  and  $Ec = 0.1, 0.3$

Figure 4 illustrates that increasing the Biot number decreases slightly the velocity but boosts temperature in the channel. Physically, a larger  $Bi$  indicates to enhanced convective heat exchange at the wall. So, there is an increase in wall temperature and consequently the buoyancy-induced motion. As  $Bi$  rises, the velocity boundary layer thickens while the temperature gradient near the wall intensifies. This indicates improved heat transfer between the surface and the fluid.

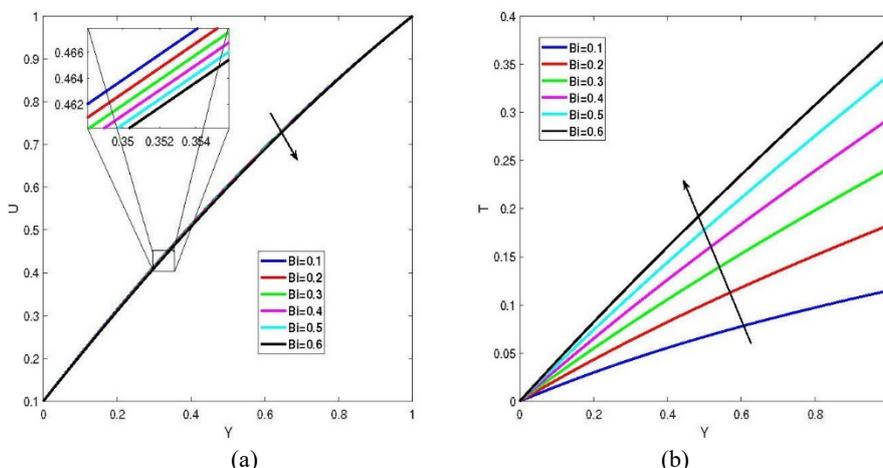


Figure 4. Effect of  $Bi$  on (a) velocity (b) temperature

Eckert number quantifies the conversion of kinetic energy into internal energy due to viscous dissipation. As shown in Figure 5, with higher  $Ec$ , the fluid experiences greater frictional heating. This leads to elevated temperature profiles and reduced velocity near the walls. The increase in thermal energy promotes stronger thermal stratification across the channel. This behaviour is consistent with the energy dissipation effects in high-shear flows.

Figure 6 shows that velocity decreases with the increase in  $\beta$ . This is due the increase in effective viscosity, particularly near the lower wall with considerable temperature gradient. Temperature distribution rises with  $\beta$ , as higher viscous resistance dissipates more energy into heat. This trend emphasizes the competing influence between viscous drag and thermal conduction in HNF systems.

Figure 7 shows that increasing the nanoparticle concentration enhances thermal conductivity of the Casson HNF. This leads to higher temperatures throughout the channel. The velocity, however, decreases with increased  $\phi$ . This is due to the rise in viscosity induced by the additional solid particles. The improved HT demonstrates the synergistic effect of Cu–Al<sub>2</sub>O<sub>3</sub> nanoparticles. They provide a better balance between viscosity increase and conductivity improvement compared to single-particle nanofluids.

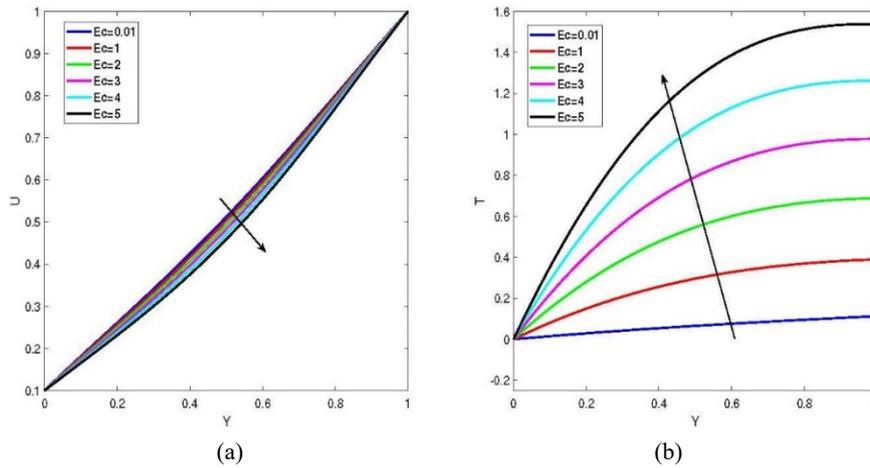


Figure 5. Effect of  $Ec$  on (a) velocity (b) temperature

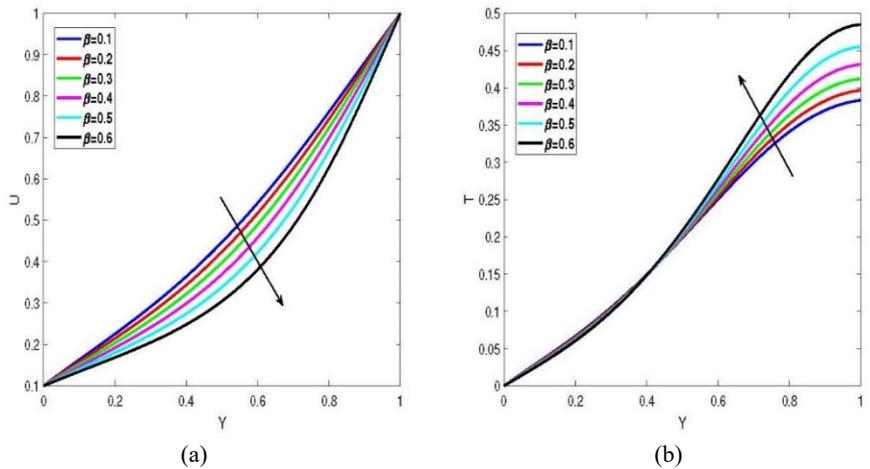


Figure 6. Effect of  $\beta$  on (a) velocity (b) temperature

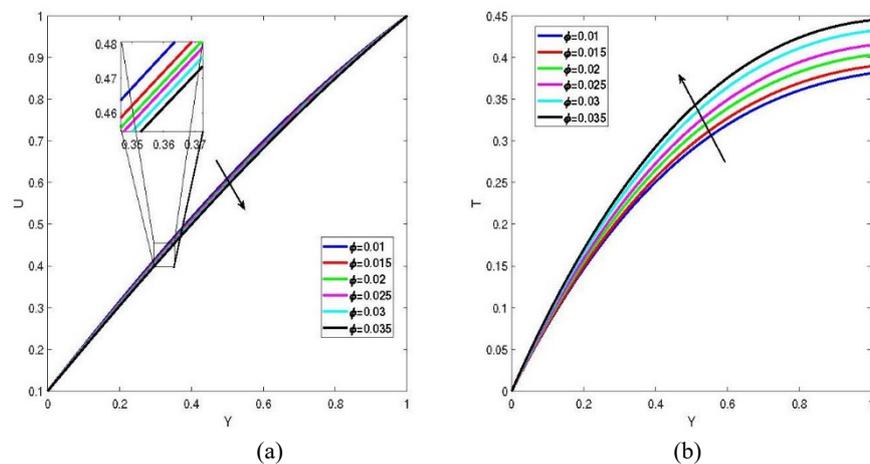


Figure 7. Effect of  $\phi$  on (a) velocity (b) temperature

From Figure 8, it is evident that increasing  $\gamma$  (the wall stretching rate) accelerates the fluid motion near the lower plate. This leads to higher velocity and thinner velocity boundary layer. The temperature decreases with the increase in  $\gamma$ .

From Figure 9, it is evident that rise in  $\lambda$  values, significantly reduces the fluid velocity and increases temperature. This is due to stronger non-Newtonian effect and higher yield stress. The suppression of motion due to yield stress restricts convective transport, and allows heat to accumulate within the fluid. This behaviour differentiates Casson fluids from Newtonian ones. It also emphasises the significance of rheology concerning HNF performance.

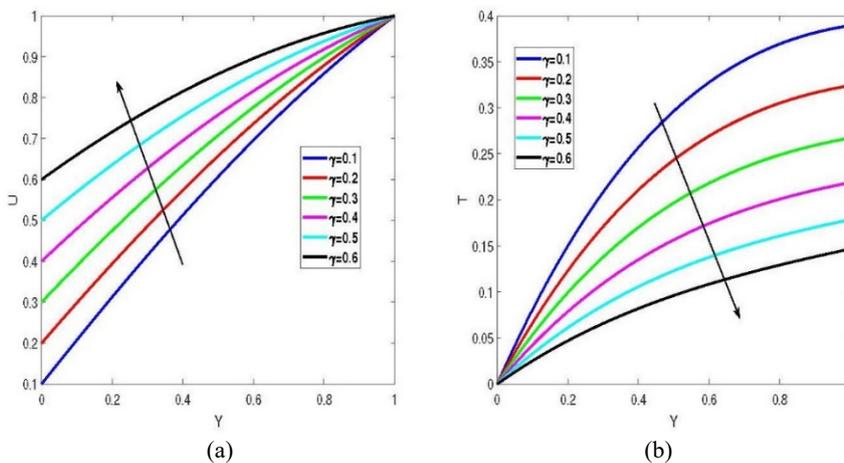


Figure 8. Effect of  $\gamma$  on (a) velocity (b) temperature

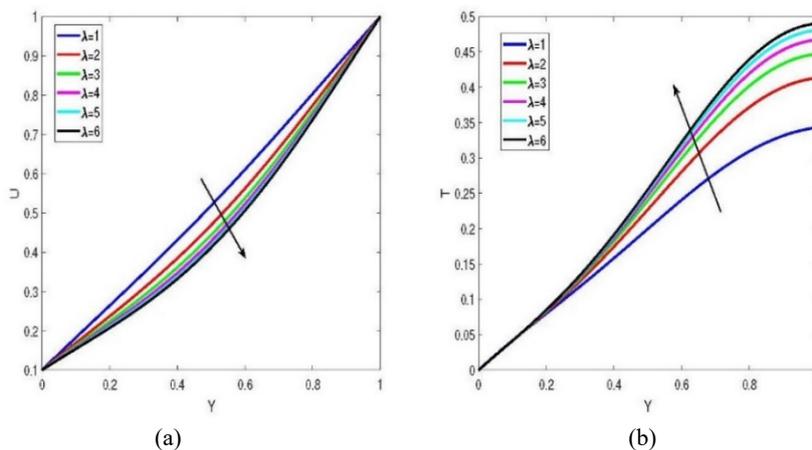


Figure 9. Effect of  $\lambda$  on (a) velocity (b) temperature

As shown in Figure 10, increasing  $Gr$  enhances velocity but decreases temperature field. This happens due to the buoyancy-driven flow formed by temperature gradients. Larger  $Gr$  values decrease the temperature slightly. When buoyancy become stronger, the warm fluid is carried away more quickly. This improves cooling effect in the channel of HNF.

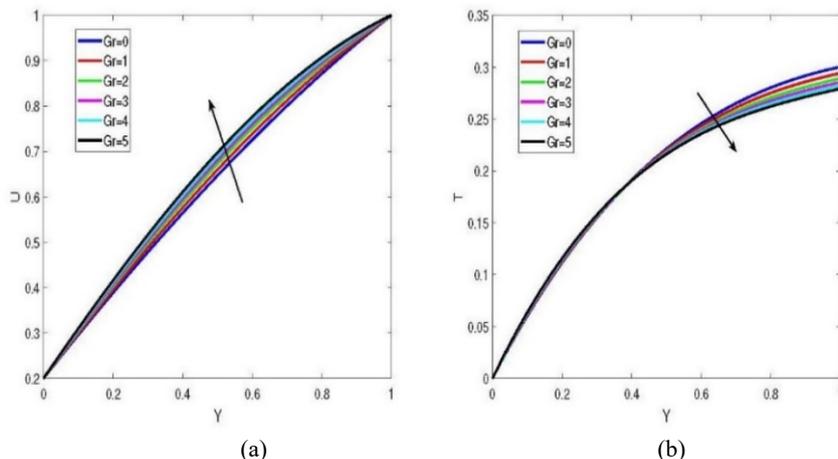


Figure 10. Effect of  $Gr$  on (a) velocity (b) temperature

Figure 11(a) shows that  $Cf_0$  decreases as the Casson parameter increases, while  $Cf_1$  rises. This means that, as the yield-stress increases weaker shear is observed at lower wall but stronger shear at upper wall. Figure 11(b) shows that  $Nu_0$  increases slightly with  $\lambda$ , while the upper wall value  $Nu_1$  decreases. This indicates that higher yield stress enhances HT at the lower plate but reduces it at the upper plate.

Figure 12(a) depicts that, as the Grashof number increases,  $Cf_0$  increases steadily while  $Cf_1$  decreases. Figure 12(b) reveals that  $Nu_0$  increases slightly with  $Gr$ , while  $Nu_1$  stays almost same with a tiny downward trend.

Figure 13 reveals that, increasing the Casson parameter  $\lambda$  raises average skin friction but reduces average Nusselt number. Increasing the Grashof number barely affects average friction but slightly boosts average heat transfer.

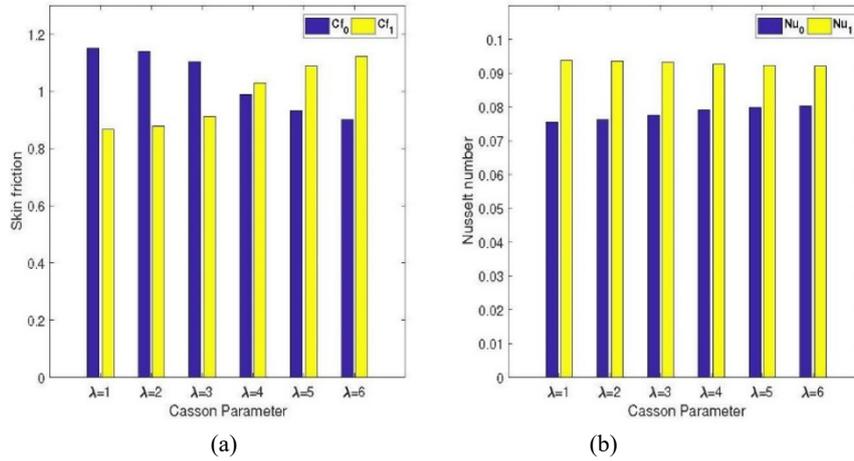


Figure 11. Effect of  $\lambda$  on (a) Skin friction (b) Nusselt number

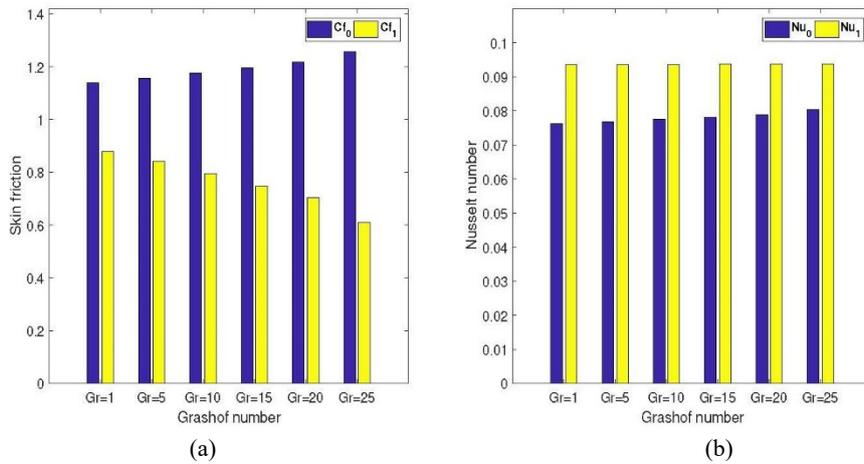


Figure 12. Effect of  $Gr$  on (a) Skin friction (b) Nusselt number

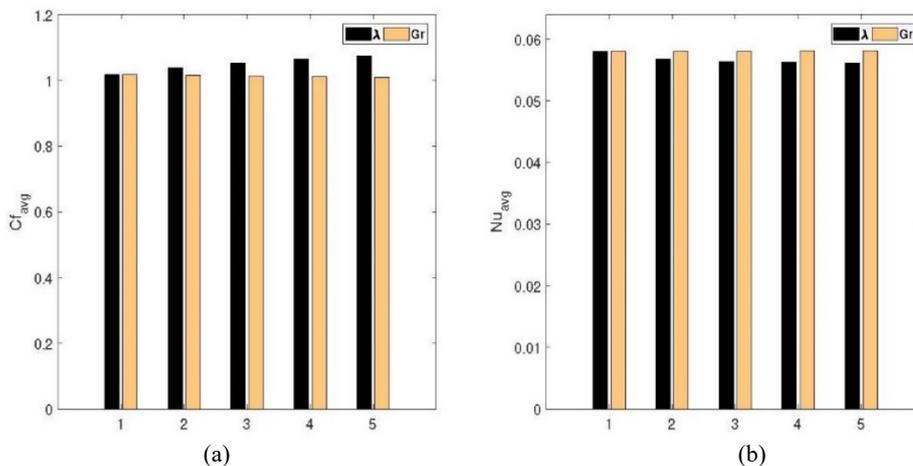


Figure 13. Variation of average (a) Skin friction (b) Nusselt number for  $\lambda$  and  $Gr$

Figure 14 illustrates the effect of time on the skin friction coefficient ( $Cf$ ) and Nusselt number ( $Nu$ ) for  $\lambda = 1$  and  $\lambda = 2$  over the time interval  $t = 0.01 - 1.05$ . It is observed that both  $Cf$  and  $Nu$  exhibit significant variations at early times, indicating transient behaviour. However, as time progresses, the variations gradually diminish, and both quantities approach constant values beyond  $t = 1$ . Therefore, in the present study,  $t = 1$  is considered as the steady state time. The time step was chosen sufficiently small  $dt = 1.3605 \times 10^{-4}$  to ensure convergence of the solution, and further reduction in the time step did not lead to any noticeable change in  $Cf$  and  $Nu$ .

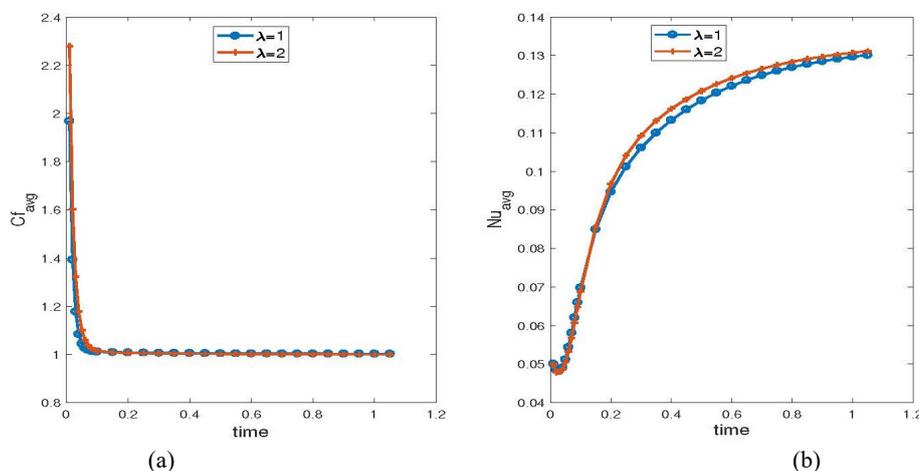


Figure 14. (a) Skin friction (b) Nusselt number for time variation and  $\lambda = 1, 2$

## 5. CONCLUSIONS

An analysis of unsteady Couette flow and HT behaviour of a Casson HNF composed of copper (Cu) and alumina (Al<sub>2</sub>O<sub>3</sub>) nanoparticles suspended in water, was carried out through numerical study. Non-dimensional governing equations were evaluated using FDM to study the effects of significant physical parameters for instance, Casson parameter ( $\lambda$ ), Grashof number (Gr), Biot number (Bi), Eckert number (Ec), viscosity parameter ( $\beta$ ), nanoparticle volume fraction ( $\phi$ ), and wall stretching parameter ( $\gamma$ ).

The findings from the study are as follows:

- The momentum field is primarily controlled by rheological and viscous parameters. Casson ( $\lambda$ ) and viscosity parameter ( $\beta$ ) exert the strongest influence on velocity and skin friction. Higher values of  $\lambda$  significantly suppress fluid motion due to increased yield stress, while larger  $\beta$  enhances viscous resistance. This indicates that non-Newtonian effects dominate momentum transport when  $\lambda$  and  $\beta$  are large.
- The thermal field is mainly governed by the Eckert (Ec) and Biot (Bi) numbers. At low Ec, HT is conduction-dominated, whereas higher Ec leads to dominant viscous dissipation, increased internal heating, thicker thermal layers, and reduced Nusselt numbers. Increasing Bi enhances wall to fluid convection, causing surface convection to dominate thermal transport.
- Buoyancy effects become important at high Grashof numbers (Gr), where natural convection speeds up the flow and improves cooling.
- Nanoparticle volume fraction ( $\phi$ ) improve heat transfer by increasing thermal conductivity but reduce fluid velocity because they increase viscosity.
- Stretching parameter ( $\gamma$ ) helps control the flow by increasing velocity near wall and reducing fluid temperature, offering useful design control for practical applications.
- From a practical perspective, the results suggest that flow resistance in HNF systems can be effectively controlled through rheological parameters  $\lambda$  and  $\beta$ , whereas thermal performance can be optimized by managing Ec and Bi. These findings provide useful design guidelines for engineering applications such as polymer processing, thermal management systems, and cooling technologies involving non-Newtonian HNFs.

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## FDM-МОДЕЛЮВАННЯ ПОТОКУ ТА ТЕПЛОПЕРЕНОСУ ГІБРИДНОЇ НАНОРІДИНИ КАССОНА Cu–Al<sub>2</sub>O<sub>3</sub>/ВОДА В СИСТЕМІ КУЕТТА

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У цій статті чисельно досліджується нестационарна гібридна нанорідина Куетта-Кассона (HNF), що містить наночастинки міді (Cu) та оксиду алюмінію (Al<sub>2</sub>O<sub>3</sub>), розчинені у воді. Верхня стінка приводиться в рівномірний рух, а нижня стінка вважається нерухомою та розтяжною. Для інтегрування керованих нелінійних диференціальних рівнянь з частинними похідними використовується метод скінчених різниць (FDM). Результати досліджуються за допомогою ліній струму, ізотерм, числа Нуссельта та поверхневого тертя. Обговорюється вплив ключових безрозмірних чисел, таких як число Грасгофа, число Біо, параметр розтягування, параметр Кассона та число Екерта, на HNF Cu–Al<sub>2</sub>O<sub>3</sub>-вода. Результати показують, що потік та теплопередача (НТ) можуть значною мірою контролюватися ключовими параметрами.

**Ключові слова:** потік Куетта; змінна в'язкість; нанорідина Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O; число Біо; параметр розтягування